1	Bioenergy Production Using Trichormus variabilis - A review
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17	Running Head: Bioenergy from Trichormus variabilis
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#### 1 Abstract

2 Fossil fuel processing and consumption contaminates air, soil, and water resources via 3 release of hazardous chemicals. To protect the environment, harnessing renewable 4 energy resources and development of sustainable technologies are prime targets of 5 research and increased investment. Use of bio-based feedstocks in energy production inherently provides a valuable pollution-curbing pathway with sustainability credentials, 6 7 especially when wastewater is used to provide the nutrient requirements. The 8 filamentous cyanobacterium, Trichormus variabilis, has attracted substantial attention 9 from researchers due to its potential for dual industrial functions in bioenergy 10 production and bioremediation. This species can efficiently use the power of sunlight 11 energy to fix atmospheric CO<sub>2</sub> for generating valuable chemical compounds, such as 12 carbohydrates and fatty acids, which can be converted to biofuels. Because it grows in 13 nutrient-rich wastewater (industrial effluent), it can serve as a bio-absorbent and replace 14 costly chemical catalysts and nano-materials classically used for removal of nutrients 15 and metals. However, no recent review has presented potential for state-of-the-art T. variabilis-driven phycoremediation-bioenergy production systems. Therefore, in order 16 to present possible routes from phycoremediation to energy production as a strategy for 17 18 developing the industrial application of T. variabilis, we present this review to bring 19 important research results on this species together and highlight major related 20 challenges and opportunities. The current status of applying algae in bioremediation and 21 production of liquid and gaseous fuels utilizing wildtype and mutants of T. variabilis is 22 explored. Finally, key points underlying potential for future research on optimization of 23 robust technologies for supplying sustainable bioenergy using this organism are 24 presented.

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26 Key words: Bioenergy, Hydrogen, Bioremediation, *Trichormus variabilis*.

#### 1 1 Introduction

2 Global economic growth over the last two centuries has largely been driven by 3 increased use of fossil fuels and was accompanied by significant environmental 4 pollution, particularly increased CO<sub>2</sub> emissions. Total world energy consumption is 5 forecast to increase by 1.4% per annum up to  $2040^{1}$ , exacerbating negative 6 environmental impacts and increasing pressure on finite fossil fuel resources. 7 Additionally, both economic growth and rises in the global population are reciprocated 8 by increased demand for freshwater required for industrial processes, agriculture, and 9 domestic use. Therefore, recycling wastewater becomes an imperative for water 10 conservation. There exist a number of routes to transform the environmental challenges 11 posed by wastewater into efficient, economically viable methods for both energy 12 production and water recycling. Phycoremediation has been used since circa 1963 as a 13 cost-effective nutrient removal method using microalgae to treat municipal wastewater<sup>2</sup>. In addition to CO<sub>2</sub> capture, phycoremediation has several other benefits, including 14 15 removal, transformation, or degradation of nutrients, organic matter, acids, metals and xenobiotic compounds, and the use of algae as an environmental monitoring system for 16 17 detection of toxic materials<sup>3</sup> and production of high-value metabolites<sup>4</sup>. Furthermore, massive biomass grown in wastewater streams can be used effectively as a promising 18 19 source of bio-fuels such as bioethanol, biodiesel, bio-hydrogen or biogas, which are 20 generally known as the most carbon neutral liquid and gaseous fuels, depending on their 21 generation technology.

22 Previous reviews have collated research on phycoremediation<sup>5</sup>, bioenergy production<sup>6, 7</sup>, biorefining<sup>8</sup> and algal photobioreactors (PBRs)<sup>7</sup>. However, to our 23 24 knowledge, none of these reviews have been dedicated to a specific strain of algae. 25 Among many microalgae species, *Trichormus variabilis* has been studied extensively 26 owing to its dual benefits: showing high potential in industrial and municipal wastewater treatment<sup>9-11</sup> and also its capability for bio-hydrogen production<sup>12, 13</sup>. The 27 worldwide distribution of T. variabilis, high auto-flocculation capacity<sup>3</sup>, tolerance of a 28 wide temperature range, and bio-fertilizer potential<sup>14</sup> strongly affirm that the study of this 29 species needs to be expanded in the future. Here, we present a comprehensive review, 30 focused on T. variabilis, and its principal enzymatic functions which make it suitable 31 32 for applications in biohydrogen production. Subsequently, we present the physico-33 chemical parameters affecting the morphology, physiology and growth of T. variabilis 34 and evaluate how these factors might impinge on the hydrogen production process. 35 Finally challenges and opportunities in developing a route to industrial application of T. 36 variabilis as a green chemistry workhorse in effluent treatment and production of 37 sustainable bioenergy are discussed.

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### 2 Methodology

40 Primary and secondary literature and data used in synthesis of this review were 41 obtained via searching Web of Science (https://clarivate.com/products/web-of-science/) 42 and PubMed (https://www.ncbi.nlm.nih.gov/pubmed/) databases and several sources of grey literature using keywords related to T. variabilis in terms of various types of 43 bioenergy and nutrient removal potential. Synonyms of T. variabilis, such as Anabaena 44 45 *variabilis*, were also used as keywords given that authors tend to use different names for this organism. Information was gathered in a two-phased process. In the first phase, 46 47 inclusion criteria were peer-reviewed academic research and published industrial pilot 48 studies or full-scale production systems. Because of paucity of published data specific

to T. variabilis no exclusion criteria were applied, except the exclusion of self-1 2 published, non-peer-reviewed material. In order to capture important data from grey literature, such as patents and technical reports, the second phase reversed the inclusion 3 4 and exclusion criteria of the first phase. The taxonomic classification of Trichormus 5 variabilis was extracted from data presented in major biological, botanical and algal databanks including AlgaeBase<sup>15</sup>, World Register of Marine Species (WoRMS ID: 6 7 146661)<sup>16</sup> and National Center for Biotechnology Information (NCBI taxonomy ID: 8 240292, https://www.ncbi.nlm.nih.gov/). Genes encoding hydrogen biosynthetic 9 enzymes (described in Section 6.3) were identified via literature and Genome Database 10 Resources of CyanoBase in Kazusa DNA Research Institute (http://genome.microbedb.jp/cyanobase/). Vector graphics were drawn by Inkscape 11 software v0.92<sup>17</sup>. To provide images of *T. variabilis* cells, algal samples were cultivated 12 13 and processed for transmission electron microscopy (TEM) as described previously<sup>18</sup>. 14 All the tables in this review were constructed from the primary results reported in 15 different studies cited within each tables. Figure 1 presents a workflow chart illustrating the search strategy used. 16

- 18 Figure 1. Flowchart of the research strategy. To develop each section of this literature 19 review, a question was formulated and related keywords generated for interrogation of 20 the databases. The returned information hit list was divided into three broad categories 21 of algal cultivation for biomass production, algal cultivation for bioenergy production, 22 and algal cultivation for phycoremediation. Progress of innovation across these were 23 critically analysed by comparative analysis and current challenges and opportunities 24 identified. Areas of future research to ensure current investments lead to commercial 25 feasibility were finally identified and discussed.
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## 3 Trichormus variabilis

28 Trichormus variabilis (syn Anabaena variabilis ATCC 29413) is a filamentous cyanobacterium from Nostocoidae subfamily<sup>19, 20</sup> found in both freshwater and within 29 soil habitats. The recorded history of study of this species begins nearly two centuries 30 ago, when it was collected for the first time in 1839 from puddles and drains in 31 32 Hooksiel and Jadebusen, located in Wangerooge Island in Lower Saxony of Germany by Kutzing<sup>21</sup>. Since then, its widespread distribution has been reported across almost all 33 continents, being a native species in many countries, from Asia to America, Africa and 34 Australia<sup>22, 23</sup>. The taxonomy of this species has faced repeated revision owing to the 35 36 formation of two main cell types (akinetes and heterocysts), including differentiation from the genus of Nostoc<sup>24</sup>, Wollea<sup>25</sup> and Anabaena<sup>19, 20, 24, 25</sup> on the basis of akinete 37 formation. According to the last rectified taxonomy (Fig. 2), it has been transferred 38 39 from Anabaena to the genus Trichormus, with the former scientific name "Anabaena variabilis" proposed by Bornet and Flahault in 1886 being replaced with "Trichormus 40 variabilis" as proposed by Komarek and Anagnostidis in 1989<sup>25-27</sup>. 41

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## Figure 2. Taxonomy of Trichormus variabilis.

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## 45 **3.1 Morphology and Physiology**

46 The filaments of *T. variabilis* are morphologically variable<sup>19, 24</sup>. Filaments mainly 47 contain chains of barrel-shaped gram-negative vegetative cells (Fig. 3a) as a site for

photosynthesis with conical terminal cells (Fig. 3b) covered by a thin gelatinous 1 2 polysaccharide sheath (Fig. 3c). The mucilaginous sheath encapsulating the filaments arises from polysaccharide secretions by the cells<sup>28, 29</sup>. Vegetative cells have a primary 3 4 role of harnessing solar energy for fixing carbon to drive biomass production. The 5 growth in biomass can be coupled to wastewater treatment through removal of heavy 6 metal ions and nutrients. The most important cell differentiation in T. variabilis is the 7 formation of heterocysts, also known as heterocytes. When transferred to diazotrophic 8 conditions, some vegetative cells differentiate into heterocysts as a site for nitrogen 9 fixation<sup>25</sup>. The spherical, ellipsoidal or cylindrical shape<sup>24</sup>, the large size<sup>25</sup>, distinctive polar bodies<sup>30</sup>, and hollow appearance, make heterocysts readily recognisable among 10 other cell types (Fig. 3d). Even though heterocysts represent only 5-10% of cells along 11 the filaments<sup>31</sup>, phylogenetic studies showed that about 45% of the genome is expressed 12 in these cells<sup>32</sup>. Cell differentiation is underpinned by changes in gene expression, 13 which trigger biochemical and structural transformations, such as formation of thick 14 15 multi-membranous glycolipid walls, arrest of photosynthesis and biosynthesis of the nitrogenase enzyme complex<sup>33</sup>. These modifications prepare heterocyst cells for the 16 17 vital role of fixing atmospheric nitrogen with hydrogen gas as a by-product of the 18 reactions. Because nitrogenase enzymes are sensitive to oxygen, heterocysts bereft of 19 oxygenic photosynthesis provide an anaerobic environment to stabilise the N-fixation 20 system in an otherwise aerobic organism. Heterocysts strongly attach to vegetative cells via cyanophycin polar nodule<sup>30</sup> (Fig. 3d). 21

In response to nutrient limitation or environmental stress such as prolonged darkness, 22 dryness, freezing, and nutrient depletion<sup>30, 34, 35</sup>, specialised akinete cells develop as 23 24 resilient archetypal spores to ensure survival of the organism in harsh environmental conditions. Akinetes are oval to barrel-shaped cells with granules filled with glycogen 25 and cyanophycin<sup>36</sup>, which can easily be distinguished from vegetative cells by their 26 larger size and thicker envelope (Fig. 3e). Their thick outer layer contains glycolipid 27 28 and polysaccharides, making them more resistant to stressful conditions in comparison to vegetative cells and heterocysts<sup>28</sup>. Akinetes germinate and develop into new filaments 29 when favourable growth conditions are restored. On germination, an akinete develops 30 31 into a short filament which is structurally distinguishable from trichorms in having 5 to 32 15 vegetative cells and lacking heterocysts (Fig. 3f). These short filaments, known as 33 hormogonia, later develop into mature trichorms possessing heterocysts. - Therefore, the 34 diverse cell functions provide an attractive system for commercial development of an 35 efficient low-cost biomass production during wastewater treatment process, which 36 could be coupled to industrial bioenergy production. The morphological appearance of 37 various cell types of T. variabilis is illustrated schematically in Fig. 3, with Fig. 4 38 showing actual images of the cells using transmission electron microscopy (TEM).

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Figure 3. Schematic depiction of different cell types of *T. variabilis.* (a)
Vegetative cells; (b) Terminal cell; (c) polysaccharide mucilaginous sheath; (d)
Heterocysts, which posses: 1. Fibrous layer, 2. Laminated layers (internal layers), 3.
Plasmodesmata, 4.Polar nodule, and 5.Thylakoids; (e) Akinete, which has: 6. sheath, 7.
additional wall, 8. Cyanophycin granule, 9. Inner layer, and 10. Dense fibrillar layer; (f)
Hormogonium; (g) Outer membrane; (h) Polyphosphate granules.

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Figure 4. Microscopic images of *T. variabilis* cells. (a) Low power light
 microscope image of filaments in nitrogen-depleted growth medium showing vegetative

cells, heterocysts, and akinete. (b) Transmission electron micrograph of filaments
encased by a gelatinous polysaccharide sheath (PC) with terminal cells (TC) at the end
of the trichorms. (c) Transmission electron micrograph showing a detached mature
vegetative cell showing peptidoglycan layer (PG), carboxysome (CS), polyphosphate
granule(PS), cyanophycin granule (CP), thylakoid and attached phycobilisomes (Tl).
Scale bars: (a) 50 µm; (b) 2 µm; (c) 500 nm.

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### 4 Physico-chemical factors affect T. variabilis biomass production

9 Knowing key physico-chemical factors required for promoting high rates of biomass 10 production is necessary for developing industrial-scale bioreactors for algal cultivation. Zho<sup>37</sup> summarized general microalgae cultivation strategies, abiotic, biotic and 11 operational factors affecting algal growth. T. variabilis is capable of growing 12 13 phototrophically, heterotrophically/chemotrophically in the dark with exogenous sugar, and also mixotrophically in light with exogenous sugar<sup>31, 38, 39</sup>. This variation in growth 14 strategy makes it a potentially favourable microorganism for use in different light- and 15 dark-driven bioenergy production processes. T. variabilis is a mild thermophilic 16 17 cyanobacterium, which has photosynthetic activity in a broad temperature range (10-35 °C) and light intensity (42- 562  $\mu$ mol.m<sup>-2</sup>.s<sup>-1</sup>)<sup>40</sup>. It was demonstrated that the growth 18 yield declined (0.1 g dry mass.g<sup>-1</sup> CO<sub>2</sub>) by increasing the initial CO<sub>2</sub> concentration from 19 4 to 18%<sup>41</sup>. Chemical nutrients, essential salts and metals directly influence different 20 21 metabolic modes, which consequently affects bioenergy yield and remediation potential. The main growth media used for T. variabilis include blue-green  $(BG)^{42}$ , Allen and 22 Arnon (AA)<sup>43</sup>, 2-(N-Morpholino) ethane sulfonic acid-Volvox (MES)<sup>44</sup>, Marin (MN)<sup>45</sup>, 23 ammonium mineral salt (AMS-1)<sup>46</sup> and Fogg's Medium<sup>47</sup>. Among these, BG and AA 24 25 are the most commonly used media, specifically when T. variabilis is used as a source 26 of bio-hydrogen. Higher biomass production was reported when grown in BG<sub>11</sub> enriched 27 with a nitrogen source<sup>48</sup>. In general, BG and AA media are based on molybdenum (Mo) 28 and vanadium (V), respectively. These two metals are required for activation of two key 29 enzymes (described in section 5.3), which are responsible for hydrogen generation. Investigating the effects of replacing Mo with V demonstrated that replacement of Mo 30 with V leads to decreases in the growth yield<sup>43</sup> while it improves hydrogen generation 31 32 vield<sup>48</sup> (section 5.4).

Experiments establishing T. variabilis growth profiles have classically used, as 33 34 accumulation. proxies biomass parameters such as photosynthetic for 35 potential/capacity<sup>49</sup> and cell density at specified wavelengths<sup>50</sup>. These have been applied in studying the effects of altering various physicochemical factors such as light and 36 nutrient supply, on T. variabilis phototrophic<sup>51, 52</sup> or heterotrophic<sup>39, 53</sup> growth. While a 37 large number of studies have investigated T. variabilis growth rate as a function of time, 38 cell density or photosynthesis components<sup>54, 55</sup>, only a few have directly surveyed the 39 interrelation between multiple parameters. Such data can be used for modelling growth 40 41 kinetics. In prior work, a kinetic model for growth of T. variabilis was developed based 42 on the Monod model as a function of  $CO_2$  and light intensity<sup>56</sup>. Predictive models are increasingly important as algal biomass generated from wastewater treatment process is 43 being used for production of biofuels when scaling-up from laboratory-scale to 44 45 industrial-scale cultures. Therefore, the model should capture key parameters affecting 46 growth rate so that bioreactor designs are optimised for maximal productivity.

47 Additionally, this species has variable morphology based on the type of mechanical48 stimulation. It normally grows as filaments that attach longitudinally to neighbouring

filaments to form thalloid structures, but when it is grown with orbital shaking, thalli formation is prevented, with a homogenous suspension of short filaments emerging<sup>43</sup>. High tendency of filaments for sticking to the walls blocks light penetration, which causes problems when cultivating this species in photobioreactors. The membranous growth form may provide an opportunity in flocculation of biomass in open raceway ponds. This potential, which resolves one of the most important challenges of industrial algal harvesting technologies in biofuel production, requires further investigation.

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### 5 Biomass production via phycoremediation

10 Providing sufficient water and nutrients, particularly low-cost nitrogen, is a challenge for large-scale microalgae cultivation for bioenergy<sup>7</sup>. However, nutrient-rich wastewater 11 streams can provide most of the nutrients required for algal growth. In addition to 12 13 utilising nitrate and phosphate, microalgae have the capacity for effective removal of 14 heavy metals. Incorporation of metals into the biomass may pose downstream risks 15 during future processing or utilisation of derivatives, depending on the uses of the 16 biomass. Owing to their rapid growth rates and potential to remove heavy metals, various microorganisms have been used in phycoremediation of municipal<sup>57</sup>, industrial<sup>58</sup> 17 agricultural<sup>59</sup> wastewaters. These microorganisms include (i) green algae; 18 or Chlamydomonas reinhardtii <sup>60</sup>, Chlorella sp.<sup>61</sup>, Nannochloropsis oculata<sup>62</sup>, Scenedesmus 19 *dimorphus*<sup>59</sup>, (ii) blue-green algae; including *Synechocystis salina*<sup>63</sup>, *Spirulina* 20 platensis<sup>64</sup>, Phormidium bohneri<sup>65</sup>, Tolypothrix ceytonica<sup>9</sup>, (iii) brown algae, including 21 Padina sp.<sup>66</sup>, Laminaria hyperborean<sup>67</sup>, and (iv) red algae such as Porphyridium 22 23 cruentum<sup>68</sup>. Among the cyanobacteria, T. variabilis has received considerable attention 24 for use in bioremediation. Attraction to this species has partly been the potential for 25 coupling wastewater treatment with production of bioenergy. The growth and 26 remediation performance of T. variabilis in treating water contaminated with 27 ammonium<sup>69</sup> and biosorption of heavy metals, such as Cr, Cd, Ni and Pb<sup>70</sup> has been 28 demonstrated. Therefore, T. variabilis is already noted as an efficient microalgae for 29 actual and potential treatment of mixed industrial and municipal wastewater<sup>9</sup>. Table 1 30 presents a synopsis of key studies on phycoremediation using T. variabilis and the 31 maximum removal efficiency reported for each process.

32 A study on phenol compounds remediation illustrated notable nitrophenol compound removal efficiency from an artificial supplemented wastewater using this species<sup>71</sup>. 33 However, since polyphenolic compounds produced by *Myriophyllum verticillatum* cause 34 35 growth inhibition of T. variabilis cells<sup>72</sup>, the feasibility and efficiency of T. variabilis 36 remedial action on phenolic contaminants will require further research. It was also 37 reported that nanomaterials, such as nano-titanium dioxide (nTiO<sub>2</sub>), have negative effect on the intracellular structure of T. variabilis<sup>73-75</sup>. Furthermore, T. variabilis growth is 38 impaired by some allelochemicals such as Harmane  $(1-\text{methyl}-\beta-\text{carboline})^{76}$  and 39 FischerellinB<sup>77</sup> causing cell lysis and photosynthesis inhibition respectively. 40 Microcystins have intense allelopathic inhibition on T. variabilis growth<sup>78</sup> and 41 differentiation of heterocysts and akinetes<sup>79</sup>. The presence of such pollutants in 42 wastewater streams affects nutrient removal efficiency by disrupting metabolic 43 44 processes and consequently, disrupts bioenergy production pathways. Therefore, more 45 research on detection of growth inhibiting pollutants, their effects, and ways to deal 46 with them is required. Exposing T. variabilis to pollutants can gradually change gene 47 expression and acclimate the organism for growth in previously toxic compounds. For 48 example, it was demonstrated that repeated cultivation of this species in a medium with

high concentration of Cu(NO<sub>3</sub>)<sub>2</sub> developed a Cu-resistant strain with broad resistance to
 Cd, Zn and Ni<sup>49</sup>. Thus, genomics and proteomics research could provide a clear
 understanding of the exact metabolic changes ubderpinning this adaptive change.

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### 6 Bioenergy production using T. variabilis

6 Several studies focused on integration of wastewater treatment and bio-fuel production using microalgal systems<sup>80-83</sup>. After nutrient removal, the biomass produced 7 can effectively be utilized as a resource for cost-effective bioenergy production. We 8 9 review the application of T. varibilis in bioenergy production from the perspective of 10 liquid (biodiesel, bio-ethanol) and gaseous (bio-hydrogen, bio-methane) bio-fuels. 11 Applying microalgae systems for bioenergy production has several environmental advantages, such as reduction of pollutant emissions and soil erosion, and economic 12 13 benefits such as tax credits and grants without competing with agricultural produce for freshwater and arable land<sup>84, 85</sup>. In addition to these general advantages, T. variabilis 14 15 has enhanced capacity for auto-flocculation<sup>3</sup> which is one of the most important 16 characteristics to decrease energy consumption during algae biomass harvesting. Also, 17 nutrient removal and CO<sub>2</sub> bio-fixation potential together with interesting cell 18 differentiations in forming heterocysts and akinetes, which provide suitable opportunities for N-fixation and growth in challenging environmental conditions, 19 respectively, and availability of processed biomass as bio-fertilizer<sup>14</sup>, suggest this 20 species may present a viable solution for algae bioenergy production with valuable by-21 22 products.

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## 6.1 Liquid bio-fuels: biodiesel and bioethanol

25 Ethical concerns about diversion of crops from the human food chain to fuel 26 production have spurred the search for inedible crop oils and waste fats for use as a bio-27 fuel feedstock. Inedible oilseeds, such as Jatropha, Castor, and other indigenous crops<sup>86</sup>, 28 <sup>87</sup> which can grow on marginal land have emerged as potential candidates. However, the 29 cost of land, labour and freshwater resources often make large-scale production 30 uneconomical when set against the yields attained. Therefore, microalgae received 31 greater attention and interest due to their capability to grow in wastewater. Since lipid 32 content is the most important key factor in utilization of oleaginous microorganisms as a 33 source of biodiesel production, considerable research focuses on increasing lipid yield. Although T. variabilis is not considered as an oleaginous species, previous reports 34 35 indicate notable increases in lipid content after exposure to environmental stress or 36 nutrient limitation. For example, it was demonstrated that lipid content of this alga in N-37 depleted Arnon medium at 30-35 °C under 12:12 h light/dark cycle was increased by ~ 2.5-fold (yield~10.5%)<sup>88</sup>. Furthermore, it has been reported that ultrasound at 200 W 38 after 5 minutes increased lipid content of T. variabilis grown in BG11 medium at 25 °C 39 under continuous illumination by 1.46-fold (yield~47%)<sup>89</sup>. Cellular stress triggered by 40 41 ultrasonic treatment was responsible for increased oil production while a longer 42 duration of treatment damaged the cells. Such stress or nutrient limitation leading to increased lipid yield was also observed in other species, including Nannochloropsis 43 sp.<sup>90</sup>, Chlorella sp.<sup>91</sup> and Chlamydomonas reinhardtii<sup>92</sup>. These useful results can be 44 45 considered as a promising solution for promoting lipid accumulation in the cells and 46 consequently enhance the biodiesel production yield. However this also requires 47 accurate investigation on the profile of fatty acid methyl esters to match the biodiesel 48 quality standards.

From a bio-ethanol perspective, T. variabilis has not been widely investigated. The 1 2 main challenge in bio-ethanol production from this filamentous species is overcoming the polysaccharide loss during processing. Research has shown that drying the biomass 3 4 using supercritical fluid followed by fermentation could increase the bio-ethanol yield 5 (24.1%) about 2-fold comparing with using lyophilization process followed by fermentation (yield~13.6%)<sup>93</sup>. A further study has confirmed that applying supercritical 6 fluid pre-treatment efficiently enhances the amount of ethanol from 1.25 g.L<sup>-1</sup> to 2.28 7 8 g.L<sup>-1 94</sup>. Evidently, more research is required to fully investigate the liquid bio-fuel 9 production potential of *T. variabilis*, especially when it is grown in wastewater.

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#### 6.2 Gaseous bio-fuels: bio-methane and bio-hydrogen

12 Biogas is the oldest form of bioenergy generated by means of methanogenic bacteria under anaerobic conditions containing ~50-70% bio-methane, which can be used as a 13 heat, power or transportation fuel<sup>95</sup>. Several microalgae have been used to combine bio-14 15 methane production with biorefinery approaches, for example, Chlamydomonas and Scenedesmus obliquus<sup>96</sup>. There are some reports of T. variabilis 16 reinhardtii biomass conversion into biogas under high temperature using anaerobic digesters 17 18 without<sup>97</sup> or in combination with immobilising technology to enhance gas production<sup>98</sup>. Methane production yield was recorded at 450 mL.g<sup>-1</sup> biomass using immobilised 19 20 methanogenic bacteria and Rhodobacter capsulatus on polymeric matrices in an anaerobic bioreactor<sup>98</sup>. In another research cumulative methane yield (64%) was 21 recorded at ~4 mmol.g<sup>-1</sup> biomass when anaerobic cellulolytic substrate were used 22 together with methanogenic Archaea from genera of Methanoculleus and 23 24 Methanosarcina<sup>97</sup>. Biogas is generated via 4 successive stages: (i) hydrolysis of 25 biopolymers to monomers, (ii) fermentation (acidogenesis) of amino acids and sugars to 26 intermediary products, (iii) acetogenesis of intermediary products to acetate, CO<sub>2</sub> and hydrogen, and (iv) methanogenesis, which transforms acetate into methane. During 27 28 anaerobic digestion, hydrolysis is known to be the rate limiting step which needs to be 29 optimized via efficient pre-treatment technologies. Owing to the composition and 30 structural features of microalgae resulting in changes in response to the different growth 31 conditions<sup>99</sup>, it is assumed that biogas production yield will be affected by *T. variabilis* 32 grown in wastewaters prior to anaerobic digestion, through expression of various 33 proteins. However, no research has yet demonstrated the effect of these generated 34 macromolecules, which consequently impact bio-degradability of biomass during 35 hydrolysis. Also, more investigation is required to be undertaken on the effect of codigestion of T. variabilis and operational conditions such as hydraulic retention time 36 and proportion of inoculum and substrates<sup>100</sup> as the main parameters known in bio-37 methane production. The results of previous studies indicated that variety and 38 39 abundance of acetate oxidizing syntrophic bacteria significantly influence conversion 40 efficiency of T. variabilis to bio-methane. Improving biogas conversion yield would be 41 an interesting subject particularly in industrial wastewater treatment plants for coupling 42 bioremediation with methane production.

The most common form of bioenergy generated from *T. variabilis* is hydrogen, a clean source of fuel that can be used either directly in internal combustion engines or in fuel cells to generate electricity<sup>101</sup>. The environmental benefits offered by renewable hydrogen are clear, particularly if the energy is being harnessed from microorganisms. Different species of algae<sup>102</sup> have been identified as potential sources of bio-hydrogen. Basic research in this field started with investigating bacterial hydrogen production in

the 1920s and later in the 1940s, attention shifted to microalgal hydrogen production<sup>103</sup>. 1 Development in applied research started in the early 1970s<sup>103</sup>. Across several species 2 used as cyanobacterial sources of bio-hydrogen<sup>104</sup>, *T. variabilis* has attracted much 3 attention owing to its 2-fold benefits in bio-hydrogen production and its considerable 4 5 potential in nutrient removal from wastewater<sup>9-11</sup>. Table 2 presents hydrogen production yield of T. variabilis under different experimental conditions. Since this species has 6 7 been widely investigated for hydrogen generation, here we focus on the biochemistry, 8 cultivation methods, and utilization of wildtype and mutant strains for 9 phycoremediation and/or fuel production.

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### 6.3 Biochemistry and genetics of bio-hydrogen generation using T. variabilis

12 Algal hydrogen production occurs via light-dependent and light-independent 13 reactions. Several articles have reviewed light- and dark-driven bio-hydrogen production<sup>105-108</sup>. The former includes bio-photolysis and photo-fermentation, which 14 15 utilise sunlight, water, and CO<sub>2</sub>, as energy, electron, and carbon sources, respectively. Light-independent hydrogen generation includes dark fermentation, which uses 16 17 carbohydrate substrates, such as found in organic waste materials. Light-dependent processes are mainly driven by photosynthesis<sup>109</sup>. Hydrogen can be generated 18 19 aerobically as a product of oxygenic photosynthesis or under anaerobic conditions, as a by-product of the conversion of organic substrates to acidogenic materials<sup>106, 110</sup>. Here, 20 21 we have reviewed H<sub>2</sub> production methods using T. variabilis with specific focus on the 22 biochemistry of enzyme systems.

The complete genome of T. variabilis ATCC 29413 was sequenced by the 23 department of energy (DOE) Joint Genome Institute (JGI)<sup>38</sup> and deposited in the 24 European Molecular Biology Laboratory (EMBL)/GenBank/ DNA Data Bank of Japan 25 26 (DDBJ) database<sup>38</sup>. The genome size is 7.1 Mbp, with a total of ~5754 predicted 27 protein-coding open-reading frames<sup>38</sup>. Availability of the full genome sequence should 28 lead to a rapid increase in our knowledge of functional genes involved in growth, 29 development, and metabolic processes in this organism. Thus, key gene networks 30 supporting the different metabolic processes in various cell types are now within reach 31 for identification.

Two enzyme systems of hydrogenase and nitrogenase play a major role in algal 32 hydrogen production<sup>106, 111</sup>. T. variabilis hydrogenase and nitrogenase enzymes and 33 genes encoding these proteins have been the subject of much research<sup>112</sup>. Hydrogenase 34 enzymes play the main role in photolysis-dependent hydrogen production as well as 35 36 hydrogen utilisation. There are two kinds of hydrogenase enzymes: (i) S-Fe hydrogenase (known as reversible or soluble hydrogenase), encoded by hoxEFUYH 37 genes<sup>113-115</sup>, function in generating molecular hydrogen to reduce NAD required for CO<sub>2</sub> 38 39 absorption in the ribulose bisphosphate cycle and (ii) Ni- Fe hydrogenase (known as uptake or membrane hydrogenase), encoded by hupSL genes<sup>116</sup>, which catalyses 40 electron transfer from molecular hydrogen to the respiratory chain. Theoretically, 41 42 efficiency of  $H_2$  production in direct photolysis is high (40.1%) but it is not practically feasible due to the high inhibitory effects of  $O_2$  on the reversible hydrogenase  $\overline{103, 106, 117}$ . 43

44 Since nitrogenase enzymes are sensitive to oxygen, this requires nitrogenase-45 catalysed H<sub>2</sub>-generating reactions to be separated from oxygen-containing 46 environments. Therefore, indirect photolysis evolved, in which hydrogen is generated in 47 two separate stages. In the first stage, electrons derived from water splitting are 48 consumed in  $CO_2$  fixation to sugars. Thus,  $CO_2$  is stored in vegetative cells as

1 carbohydrate and then transported to heterocysts, where the sugar is used as an electron donor<sup>118, 119</sup>. In the second stage, breakdown of the sugar releases electrons used to 2 produce hydrogen by nitrogenase enzymes<sup>103</sup>. In the heterocysts of T. variabilis, groups 3 4 of *nif* and *vnf* genes are expressed to give rise to metal ion-dependent nitrogenase, 5 which is responsible for nitrogen fixing and generates hydrogen as a by-product of the process. There are three main gene clusters encoding nitrogenases, depending on 6 7 distinct prosthetic groups: Mo-Fe (nif1 and nif2 genes), V-Fe (vnf genes) and Fe-Fe (anf 8 genes) nitrogenases. Mo-Fe nitrogenases are encoded by (i) groups of nif1 genes, including *nifBSUHDKENXW*<sup>20, 120-123</sup> and three open reading frames expressed under 9 10 diazotrophic conditions, and (ii) nif2 genes expressed under anoxic conditions. The latter are essentially the same (nifBSUHDKENXW) genes with the exception of a few 11 12 differences, such as the fusion of *nifX* and *nifEN* genes into a single open reading frame<sup>124</sup>. V-Fe nitrogenase contains  $\alpha\beta\delta$ -subunits and scaffold proteins encoded by 13 vnfDKGENH<sup>125</sup> which is expressed under diazotrophic conditions in the absence of Mo. 14 15 with or without V. The third nitrogenase known as Fe-Fe nitrogenase is encoded by anfHDGK<sup>126</sup>. Further reviews and reports of T. variabilis nitroganase gene expression 16 and heterocyst metabolism have been published<sup>124, 125, 127-131</sup>. Although indirect 17 18 photolysis is more feasible than direct photolysis, the H<sub>2</sub> production efficiency is lower 19 (16.3%) due to the multiphase process and ATP consumption required to drive the nitrogenase activity<sup>103</sup>. 20

Other options based on fermentation of biomass have been developed. Hey et  $al^{132}$ 21 22 reviewed key factors affecting photo and dark fermentation, including substrates, inoculum density, and environmental conditions. Light fermentation is similar to 23 24 indirect photolysis. During indirect photolysis, endogenous organic compounds are used 25 to produce hydrogen, while in photofermentation exogenous organic compounds are 26 consumed for use in generating electrons. Thus, fermentation is considered the most 27 promising method for microbial  $H_2$  production<sup>103</sup>. Unlike light driven processes, during 28 dark fermentation organic substrates are used both as energy and electron sources. Bartacek et al<sup>133</sup> summarized fundamentals of fermentative H<sub>2</sub> generation in different 29 30 microorganisms. Although anaerobic bacteria are mostly used in dark fermentation, it 31 was reported that the combination of photo and dark fermentation of photosynthetic bacteria and algae could significantly enhance the bio-hydrogen productivity<sup>134</sup>. To the 32 best of our knowledge, there are no reports on application of T. variabilis in such a 33 34 hybrid system. Thus, further research on metabolic pathways of dark-driven hydrogen 35 generation using T. variabilis is required.

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#### 6.4 Factors affecting H<sub>2</sub> generation in *T. variabilis*

38 Maximal H<sub>2</sub> production from algal cultures can be achieved through optimisation of 39 key physicochemical factors with a regulatory influence on the generation capacity. 40 High light intensity inhibits H<sub>2</sub> production rate due to up-regulation of photosynthesis, which enhances oxygen accumulation and consequent inhibition of nitrogenases<sup>104, 135</sup>. 41 42 Darkness, on the other hand, can block H<sub>2</sub> production via depletion of carbohydrate 43 reserves, which triggers a deficiency of energy and electrons needed for nitrogenase activity<sup>118, 136</sup>. The negative effects of excessive oxygen can be overcome through 44 degassing or generating a partial vacuum<sup>137</sup>, sparging with argon gas<sup>138</sup> and temporal 45 separation of the photosynthetic phase from the  $H_2$  generation stage<sup>48</sup>. Based on the 2-46 stage system for H<sub>2</sub> production, a flat panel photo-bioreactor was found to increase 47 biomass production in the first stage with N-replete medium, and the H<sub>2</sub> generating in 48

1 the second stage with N-depleted medium sparging with pure  $Ar^{48}$ .

2 The presence of a nitrogen source in the growth medium severely decreases  $H_2$ 3 production, particularly when the nitrogenase enzyme machinery is the dominant H<sub>2</sub>-4 producing complex. This is because inorganic nitrogen suppresses differentiation of 5 heterocysts, thereby removing heterocyst-dependent generation. Although H<sub>2</sub> could be generated as a by-product of N-fixation utilizing atmospheric nitrogen as noted earlier 6 7 (section 5.3) and the frequency of heterocysts increases in N-free growth medium<sup>139</sup>, the 8 innate biochemical inefficiencies of this process reduce H<sub>2</sub> gas production. About 75% 9 of electrons are diverted away from H<sub>2</sub> synthesis to ammonium reduction, and this loss 10 can be averted by the absence of atmospheric nitrogen<sup>118</sup>.

 $H_2$  production rate diminishes with decreasing pH<sup>140</sup>. A study focusing on pH effects 11 demonstrated that algal growth rate was 3 times higher in the presence of Mo- or V-12 13 nitrogenase than in the presence of Fe- nitrogenase and maximum H<sub>2</sub> production was attained in the presence of V-nitrogenase in a wide range of alkaline cultures (pH 7-14 15 9)<sup>141</sup>. Mo and V are required as essential components in Mo-nitrogenase and Vnitrogenase based H<sub>2</sub> production, respectively, provided in BG and AA growth media<sup>118</sup>, 16 <sup>142</sup>. Although Mo significantly increases  $H_2$  production rate, it has a specific upper limit 17 (1.6 mM) beyond which further increases do not influence productivity<sup>118</sup>. The 18 19 maximum light to hydrogen energy conversion efficiencies were achieved in Allen-Arnon media, where a larger heterocyst frequency was noted<sup>48</sup>. Temperature is another 20 21 parameter affecting H<sub>2</sub> photo-production. A short-term thermal stress (30-36 °C) enhances nitrogenase activity of T. variabilis<sup>143</sup>. The results of studying  $CO_2$ 22 concentration, as a carbon source, demonstrated that an optimum initial CO<sub>2</sub> molar 23 24 fraction of 0.05 is required for maximum biomass production<sup>56</sup>. Additionally, inclusion of a carbon source, such as glucose, gives rise to further hydrogen production<sup>118</sup>. 25

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#### 6.5 Genetic approach for increasing *T. variabilis* H<sub>2</sub> production

28 Manipulation of the parameters dealt with in the preceding section (e.g., pH, 29 temperature, and nutrients) can be used to increase hydrogen production by algal 30 systems. However, substantial research efforts have been directed at other key targets to 31 enhance hydrogen yield. For example, the reversible hydrogenase enzyme system, 32 which can consume as well as generate hydrogen, is an obvious target for inactivation 33 using genetic approaches. Similarly, the uptake hydrogenase, which only consumes  $H_2$ 34 can be targeted for gene deletion. Accordingly, a T. variabilis loss-of-function mutant (AVM13) in the hupSL gene, which encodes the uptake hydrogenase, had at least a 3-35 fold increase in  $H_2$  production when compared to the wildtype<sup>144</sup>. Nitroso-guanidine 36 37 mutagenesis was used to generate PK84 and PK17R T. variabilis mutants with loss-offunction mutations impairing uptake hydrogenase in both mutants and an additional 38 impairment of bidirectional (reversible) hydrogenase in PK84<sup>145</sup>. When compared to the 39 wildtype, H<sub>2</sub> production in PK17R and PK84 was increased 1.4-fold and 4.3-fold, 40 respectively<sup>146</sup>. Notably, while wild-type strains produce appreciable amounts of  $H_2$ 41 only in an argon atmosphere (to preclude  $O_2$ ), the mutant PK84 produced  $H_2$  in a  $CO_2$ 42 43 atmosphere, which is more desirable from a process scale-up perspective<sup>147</sup>. While mutants are showing great promise (Table 2), environmental concerns about the release 44 of genetically modified organisms exist<sup>148</sup>. Since open biomass production systems are 45 likely to be used in combined phycoremediation and bioenergy generation, use of 46 47 mutant algae is inevitably problematic.

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### 6.6 Feasibility of integrated biofuel production and wastewater treatment

2 In order to make the application of microalgae system feasible at industrial scale, it is 3 vital to use sunlight as an energy source to significantly reduce the operation costs, 4 relative to using artificial lighting. The mutant form of T. variabilis has demonstrated viable growth in ambient outdoor conditions<sup>149-151</sup>. It was shown that in such conditions, 5 this species can prolong hydrogen generation without medium refreshment for 40 6 7 days<sup>151</sup>. Also the feasibility of growing the wildtype of this species in wastewater had 8 promising results<sup>9</sup>. Although there are some pilot studies concentrated on bioenergy 9 production and/or wastewater treatment using T. variabilis, there still is lack of specific research examining performance at larger industrial scale. However, several research 10 11 groups have demonstrated that under certain circumstances, large-scale H<sub>2</sub>-photo production using microalgae is viable<sup>152</sup>. Previously, scaling up the algal systems for 12 bioenergy production was investigated from different techno-economic and socio-13 environmental angles considering various parameters, such as water and energy 14 15 consumption, cultivation and harvesting technologies, and associated costs and 16 savings<sup>84</sup>. Open raceway ponds with lower capital and operational costs, in comparison to PBRs, represent an attractive option for commercial large-scale bioenergy 17 18 production<sup>153</sup>. It was demonstrated that this technology provides a "win-win strategy"<sup>154</sup>, having remarkable productivity with an average capacity of 40-70 tons 19 biomass.ha<sup>-1</sup>.year<sup>-1</sup> during bioremediation process, which can be coupled with 20 biorefinery<sup>153</sup>. Results of a feasibility study for integration of wastewater treatment and 21 biogas production using microalgae systems indicated positive benefits on payback 22 23 period and internal rate of return (IRR) for biofuel production when considering 24 environmental revenue and cost-savings, such as bio-products income, carbon credits and wastewater treatment<sup>155</sup>. The same strategy was reported as a feasible solution for 25 26 using algae and bacteria cocultures to couple bioremediation and biofuel production <sup>156</sup>. Economic feasibility of commercial raceway pond use in wastewater treatment and 27 28 biogas production should consider the pond size, electricity requirements, and thermal capacity for bio-methane production<sup>157</sup>. In such a system, the required  $CO_2$  and thermal 29 energy could be met by generation via combined heat and power production (305 kg 30 CO<sub>2</sub>.d<sup>-1</sup> and 488 kWh.d<sup>-1</sup>) coupled with biogas production system<sup>157</sup>. Therefore, the 31 32 limited information on feasibility of bioenergy production using microalgal systems 33 points to a beneficial outcome with significantly reduced energy consumption and costs 34 if the system integrates with bioremediation to cover nutrient (40-100 kg of N and 3-12 kg of P) and water (11–13 ML.ha<sup>-1</sup>.year<sup>-1</sup>) requirements<sup>153</sup>. 35

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### 7 Challenges and opportunities

There are several studies on various aspects of *T. variabilis* biology, cultivation, and application to phycoremediation. Here, we have provided a coherent synthesis of the literature by presenting how surveying the interrelation between different studies could develop a route to industrial application of *T. variabilis* in bioremediation and production of sustainable bioenergy, discussing challenges, opportunities and research gaps as bellow:

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45 1) Bioremediation performance of *T. variabilis* illustrated promising results in bioabsorption of nutrients and heavy metals such as Cu, Zn, and Ni. Remediation of different metals may influence gene expression and enzymatic function. This would be more important when the biomass harvested from remediation process

is used directly for bioenergy production. Thus, research into the effects of remediation on metabolic pathways, which control bioenergy generation, in this species needs to be undertaken.

- 4 2) There are some pilot studies showing the utility of *T. variabilis* in bioremediation 5 using artificially constituted "wastewaters". However, actual wastewaters may contain unknown hazardous compounds and allelochemicals, which can 6 7 negatively influence algal growth. For example, nTiO<sub>2</sub>, Microcystins, Harmane 8 and FischerellinB restrict application of algae in wastewater streams containing 9 such pollutants. Therefore, it is necessary to examine actual biomass generation in different real wastewater streams for scaling up phycoremediation at industrial 10 scale for biorefining purposes. 11
- 12 3) The application of *T. variabilis* for biodiesel and bio-ethanol production has not been widely studied. Although T. variabilis is not considered an oleaginous 13 species, environmental stress can induce cells to produce significant amounts of 14 15 lipid. The molecular genetic basis for the enhanced lipid synthesis requires further research. Also, bio-ethanol production using this organism is not viable 16 17 due to the challenge of polysaccharide loss together with associated costly and 18 high energy-consuming technologies required for the process. Therefore, more efficient solutions are required. 19
- 4) Biogas generation using this alga is promising, particularly when coupled to 20 21 wastewater treatment. In order to improve bio-methane yield, first it is necessary to evaluate the effect of the bioremediation process on algal cell composition, 22 23 protein profile and biomass bio-degradability. This would provide valuable 24 information to boost the initial hydrolysis processes via applying the most 25 appropriate pretreatment technology. Also, applying co-digestion technologies 26 can enhance anaerobic digestion kinetics and, from an economic aspect, there 27 are still several improvement methods such as optimizing the proportions of 28 microalgal cells for declining the anaerobic digestion hydraulic retention times 29 which need further investigation.
- 5) Bio-hydrogen production using T. variavilis is focused on light-driven methods 30 and the potential of using this species in dark-driven hybrid systems, particularly 31 32 in combination with dark fermentation, has not yet been surveyed. Although the 33 challenge of oxygen inhibitory effects on hydrogen generation can be averted by degassing, partial vacuum, sparging Ar, applying two-staged H<sub>2</sub> generation 34 35 method or utilysing mutants of T. variabilis, presented solutions are costly and carry environmental risks. Therefore, still further research is necessary to 36 37 develop cost-effective and environmentally friendly alternatives for robust bio-38 hydrogen production systems.
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# 8 Future prospects

41 In this review, we have sought to collate the wide literature on *Trichormus variabilis*, 42 bringing data together from many different aspects, including morphology focusing on 43 different types of cell differentiation and physiology, together with a review of growth parameters and conditions where the species may be used in remediation of wastewaters 44 45 coupled with production of different forms of liquid and gaseous bioenergy, such as 46 biodiesel, bio-ethanol, bio-methane and bio-hydrogen. We attempted to distil the key information available on T. variabilis on phycoremediation and bioenergy production to 47 enable further research on optimization of robust technologies for supplying clean water 48

and sustainable energy resources. Trends in research of T. variabilis during the last 1 2 decades has focused on the main aspects of (i) biology, (ii) nutrient removal and (iii) bioenergy production, and considered the effects of several stress factors on growth and 3 4 lipid production. There is a promising path for future application of this species even 5 though there are still major environmental and economic issues which need to be resolved to optimise T. variabilis for industrial usage. The valuable potential of this 6 7 microorganism arising from the differentiation of vegetative cells into other cell types 8 for adaptive responses to different environmental conditions provides a great 9 opportunity to develop platforms for commercial exploitation of this species. It is 10 important to elucidate the mechanisms of cell differentiation and metabolic changes 11 associated with exposure to stress.

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### 17 Competing interests

18 The authors have no competing interests.

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6

Experimental conditions	Removed compounds	Efficiency (%)	Ref
<b>Preliminary growth:</b> MBL medium, 25–35 °C, day light for 14 days.	BOD	89.3	9
Treatment process: Mixed domestic-industrial wastewater, 25–35 °C,	COD	52.6	
daylight.	TSS	44.6	
	TDS	38.8	
	Fats, Oil and Grease	68.2	
	Zn	81.2	
	Cu	91	
<b>D</b>	DOD	02	10
<b>Preliminary growth:</b> BG <sub>11</sub> medium, 30 °C for 15 days.	BOD	83	10
<b>I reatment process:</b> ~16% of BG <sub>11</sub> medium mixed with textile industry	COD	15	
effluent wastewater for 25 days, 30 °C, aerobic condition.	SO4	55.4	
	N1	63	
	Zn	67	
	Ca	17.5	
	Mg	28	
Preliminary growth: MDM medium.	<i>o</i> -Nitrophenol	100	71
27.5 °C, ~ 65 $\mu$ mol.m <sup>-2</sup> .s <sup>-1</sup> , aerated containing 1% CO <sub>2</sub> for 7 days.	<i>m</i> -Nitrophenol	100	
<b>Treatment process:</b> using supplemented medium, phenols concentration	<i>p</i> -Nitrophenol	4	
40 µM, 25 °C for 120 h.	2.4-Dinitrophenol	95	
	2.4.6-Trinitrophenol	51	
	Bisphenol A	23	
<b>Preliminary growth:</b> Fogg medium, $24 \pm 1$ °C, ~ 55µmol.m <sup>-2</sup> .s <sup>-1</sup> , 16 h light / 8 h dark cycle for 22 days.	Zn	85.1	158
<b>Treatment process:</b> supplemented medium, Standard stock solution of $Zn^{2+}$ ions (1000 $\pm 2$ mg.L <sup>-1</sup> )			

 Table 1. Bioremediation potential using T. variabilis.

<b>Preliminary growth:</b> calcium alginate immobilized cell <b>Treatment process:</b> supplemented medium, 11-10 ppm concentration of	Pb	96	159
lead			
<b>Preliminary growth:</b> Chu-10 medium, $28 \pm 2 ^{\circ}$ C, daylight ~ 45 µmol m <sup>-2</sup> s <sup>-1</sup>	Cr	54	160
<b>Treatment process:</b> supplemented medium, Stock solutions of chromium concentrations of (10 - 100 mM) prepared by dissolving K <sub>2</sub> Cr <sub>2</sub> O <sub>7</sub> .			
<b>Preliminary growth:</b> Allen and Arnon medium, 25 °C, 15 µmol.m <sup>-2</sup> .s <sup>-1</sup> <b>Treatment process:</b> Ammonium ions were added in concentration of 0.5 mg.L <sup>-1</sup> , immobilized cells in the photobioreactor for 25 days.	Ammonium	90	13

Strain (wild/mutant)	Experimental conditions	Medium	Hydrogen production rate	Ref
ATCC 29413	Growth: 30 °C, 60 $\mu$ mol.m <sup>-2</sup> .s <sup>-1</sup> H <sub>2</sub> : 5% CO <sub>2</sub> , Ar (25 ml min <sup>-1</sup> ), 35 °C, 70 $\mu$ mol.m <sup>-2</sup> .s <sup>-1</sup> , (a) 1.6 mM Mo, (b) 10 mM glucose	$BG_0$	<ul> <li>(a) 44 μmol.mg chla<sup>-1</sup>.h<sup>-1</sup></li> <li>(b) 49 μmol.mg chla<sup>-1</sup>.h<sup>-1</sup></li> </ul>	118
	Growth: 95% air + 5% CO <sub>2</sub> , 30 °C, 65 $\mu$ mol.m <sup>-2</sup> .s <sup>-1</sup> H <sub>2</sub> : Ar (45 ml min <sup>-1</sup> ), 30 °C, 150 $\mu$ mol.m <sup>-2</sup> .s <sup>-1</sup>	BG <sub>0</sub>	0.9 mL.g dry cell $^{-1}$ .h $^{-1}$	48
	Growth: 30 °C, 35-161 µmol.m <sup>-2</sup> .s <sup>-1</sup> , 190 rpm H <sub>2</sub> : 100% Ar	BG11 AA BG11	1 mL.g dry cell <sup>-1</sup> .h <sup>-1</sup> 5.6 mL.g dry cell <sup>-1</sup> .h <sup>-1</sup> ~6 mL.g dry cell <sup>-1</sup> .h <sup>-1</sup>	41
	Growth: Ambient air, 25 °C, 5 µmol.m <sup>-2</sup> .s <sup>-1</sup> (bottom), 15 µmol.m <sup>-2</sup> .s <sup>-1</sup> (surface) H <sub>2</sub> : 100% Ar, Hydrophilic cuprammonium rayon hollow fibers PBR, medium was heated at 50°C prior injection	AA	17- 20 mg.g dry cell <sup>-1</sup> .h <sup>-1</sup>	13
	Growth: ~ 67.5 $\mu$ mol.m <sup>-2</sup> .s <sup>-1</sup> H <sub>2</sub> : Ar + 5% CO <sub>2</sub> , 77 mM Tween 85	AA	$0.44 \pm 0.03$ mL.mg dry cell <sup>-1</sup> .h <sup>-1</sup>	161
CCAP 403/4B	Growth: 1.7% CO <sub>2</sub> , 28 °C, continues 45-55 $\mu$ mol.m <sup>-2</sup> .s <sup>-1</sup> , 140 rpm H <sub>2</sub> : Vacuum degassed (270-300 torr),170-180 $\mu$ mol.m <sup>-2</sup> .s <sup>-1</sup> for 5 hr	$AA_0$	12 .5 mL.g dry cell <sup>-1</sup> .h <sup>-1</sup>	140
	Growth: Air without CO <sub>2</sub> , 28 °C, 15 μmol.m <sup>-2</sup> .s <sup>-1</sup> , 140 rpm H <sub>2</sub> : No gas phase, cells immobilized on hollow fibers; 25 μmol.m <sup>-2</sup> .s <sup>-1</sup> (surface), 13 μmol.m <sup>-2</sup> .s <sup>-1</sup> (bottom), medium was heated at 50 °C prior injection	$AA_0$	20 mL.g dry cell <sup>-1</sup> .h <sup>-1</sup>	137

 Table 2. Hydrogen production yield using *T.variabilis* under different experimental conditions.

PK84	Growth: Air + 2% CO <sub>2</sub> ( 500 mL.min <sup>-1</sup> ), 12 h light (36 °C)/ 12 h dark (14- 30 °C) H <sub>2</sub> : (a) air, (b) air+ 2% CO <sub>2</sub> , (c) 80% Ar + 20% O <sub>2</sub> , (d) 100% Ar, 332 µmol.m <sup>-2</sup> .s <sup>-1</sup>	AA <sub>0</sub>	(a) $106.0 \pm 7.0 \ \mu \text{mol.mg chla}^{-1}.\text{h}^{-1}$ (b) $81.0 \pm 10.0 \ \mu \text{mol.mg chla}^{-1}$ <sup>1</sup> .h <sup>-1</sup> (c) $190.0 \pm 8.0 \ \mu \text{mol.mg chla}^{-1}$ <sup>1</sup> .h <sup>-1</sup> (d) $191.0 \pm 11.0 \ \mu \text{mol.mg chla}^{-1}$ <sup>1</sup> .h <sup>-1</sup>	149
	Growth: Air+ 2% CO <sub>2</sub> (500 mL.min <sup>-1</sup> ) H <sub>2</sub> : Outdoor PBR, ~ 1.84 mol.m <sup>-2</sup> .s <sup>-1</sup>	$AA_0$	80 mL.h <sup>-1</sup> .PBR $v^{-1}$	150
	Growth: air + 2% CO <sub>2</sub> (500 mL.min <sup>-1</sup> ), 30 $^{0}$ C H <sub>2</sub> : Outdoor PBR, sun light	$AA_0$	$60-140 \text{ mL.h}^{-1}.\text{PBR v}^{-1}$	151
(a) ATCC29413 (b) PK84	Growth: air + 2% CO <sub>2</sub> (0.5 L.min <sup>-1</sup> ), 30 <sup>0</sup> C, 113 μmol.m <sup>-2</sup> .s <sup>-1</sup> H <sub>2</sub> : 100% Ar, 30 <sup>0</sup> C, 200 μmol.m <sup>-2</sup> .s <sup>-1</sup>	AA	<ul> <li>(a) 39.4 nmol.μg chla<sup>-1</sup>.h<sup>-1</sup></li> <li>(b) 32.3 nmol.μg chla<sup>-1</sup>.h<sup>-1</sup></li> </ul>	135
<ul> <li>(a) ATCC29413</li> <li>(b) PK84</li> <li>(c) PK17R</li> </ul>	Growth: 25% N <sub>2</sub> , 2% CO <sub>2</sub> , 73% Ar (250 mL.min <sup>-1</sup> ), 90 μmol.m <sup>-2</sup> .s <sup>-1</sup> H <sub>2</sub> : Ar, 30 <sup>0</sup> C, 140 μmol.m <sup>-2</sup> .s <sup>-1</sup> , N/C starvation	$AA_0$	(a) 1.62- 3.07 nmol. $\mu$ g prot <sup>-1</sup> .h <sup>-1</sup> (b) 6.91-12.6 nmol. $\mu$ g prot <sup>-1</sup> .h <sup>-1</sup> (c) 2.24-4.10 nmol. $\mu$ g prot <sup>-1</sup> .h <sup>-1</sup>	146
AVM13	Growth: Air, 1% CO <sub>2</sub> , 30 $^{0}$ C, 100 µmol.m <sup>-2</sup> .s <sup>-1</sup> H <sub>2</sub> : Washed with N-free medium	$BG_0$	68 nmol. $\mu$ g <sup>-1</sup> .chl $a^{-1}$ .h <sup>-1</sup>	144